

Maximization of Oil Production in the Norne Field C-Segment: Well Placement Comparative Study

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Abstract—Maximum oil production can be obtained with more oil wells, but few optimal numbers of wells in good location reduces economic costs and increase recovery. In this work, The Norne field C-segment reservoir model in Eclipse® software is used to study the effect of well placement. Six producers (while the four injectors remain the same as those of the base case) for two different well placement scenarios, 1 and 2, are located manually after identifying grid blocks with high oil saturation from an updated geological model. Insignificant variation in oil recovery factors, 1.3%, is obtained for the base case and the two scenarios. However, after taking into account the well costs, gas and water injection costs under reasonable economic assumption, the NPV results shows that scenario 2 with the highest NPV is considered to be more favourable.

Keywords—Maximum Oil production, Well placement, Norne field C-Segment, Reservoir Simulation, Oil Recovery, Economic Analysis, Net Present Value.

I. INTRODUCTION

The Norne database in the Center of Integrated Operation in the Petroleum industry at the Norwegian University of Science and Technology (NTNU) has a license limitation but it is readily available for postgraduate research projects. Many academic projects, mostly simulation of chemical EOR processes to improve oil recovery from Norne field, have been carried out at the Center of Integrated Operation in the Petroleum industry at the Norwegian University of Science and Technology (NTNU) by utilizing the Norne database.

However, this work studies the effect of well placement for maximum oil recovery in the Norne Field C-segment. Determining the best location for new wells is a complex problem that depends on

reservoir and fluid properties, well and surface equipment specifications, and economic criteria. Placing too many wells in oil reservoir is known to have tremendous effect in oil recovery but it has also cause increase in economic cost in the oil industry for many years now. Optimum well placement most of the time is done based on a deterministic (most likely) case. In this sense, the use of reservoir simulation allows the engineer to evaluate different placement scenarios.

A total number of ten wells; six producers and four injectors are placed in each scenario. In order to obtain maximum oil recovery, the producers are placed horizontally while injectors remain the same as those from the base case. The new well placements in the scenarios are identified with the suffix "P-H" for producers and "I-H" for injectors. Simulation results, the total oil produced for wells in each scenario from the start year 1997 to December 2015 are reported.

The Net present values for the three cases are then calculated taking into account the economic costs such as well cost, cost of gas and water injection. Sensitization was done on the oil price (\$25, \$35). The NPV results are discussed and the most economical well placement scenario is thus identified.

II. THE NORNE FIELD AND ITS SIMULATION MODEL

The Norne field, one of the largest discovery on the Norwegian continental shelf in more than a decade with recoverable oil reserves of 450 Mbbl, has four main fault blocks of C, D, E and G segment. The Norne Main Structure (Norne C-, D- and E-segment, discovered in 1991) contains 97% of the oil in place. The Norne field is in Blocks 6008/10 and 6508/10 on a horst block in the southern part of the Nodland II area in the Norwegian Sea. The drainage strategies/drive mechanisms on the field are pressure depletion, gas injection, water injection and combine gas and water injection. Based on the framework, water and gas

injection is recommended as the base mechanism for the C-segment field. The rocks within the Norne reservoir are Late Triassic to Middle Jurassic. The current geological model has five reservoir zones-Garn, Not, Ile, Tofte, and Tilje. Oil is found mainly in the Ile and Tofte formations, and gas is found in the Garn formation. The sandstones are at a depth of 2500m to 2700m. The porosity ranges from 25 to 30%, and permeability varies from 20md to 2500md. The data consist of near-, middle-, and far-stack 3D-seismic data acquired in 2001, 2003, and 2004.

The Norne field has been simulated by four different Eclipse black oil models, from oldest to newest [13, 14]. New simulation models are built when significant updates of the geological model are done, or if certain formation needs refinement. The reservoir model used in this work is the 2004 geological model with 3D three-phase full field black-oil model. The Norne full field model consists of 49080 active grid cells. DX & DY range between 80 – 100 m. The Norne C-segment coarsened grid model was separated from the rest of the field by keeping the C-segment coarsened model with 29x49x22 grid blocks active. Water compressibility of 4.67×10^{-5} /bar at 277 bars and rock compressibility factor of 4.84×10^{-5} /bar are used in the model. The formation volume factor used is 1.038 Rm³/Sm³ and the oil viscosity is 0.318 cp.

III. WORK FLOW

This section explains the base case which is defined as the initial case obtained from Eclipse 100 simulation run from Statoil. The scenarios 1 and 2 are created based on the initial field reservoir conditions (rock and fluid properties) at 1997. New wells are placed manually on high oil saturation on the scenario cases and the results obtained on well placement and oil production will be compared for economic benefit.

A. Base Case

The total number of wells located on the base case is 13, 9 producers and 4 injectors from the simulated model of the field from the duration of 1997 to 2006. More also, the work will predict production until 2015. In the base case the producing well and injection wells used a template name B, D, K and C respectively. Well locations on the base case are based on the following principles [15]:

- Water injectors are located at the flanks of the reservoir
- Gas injectors located at the structural heights of the reservoir.
- Oil producers located between gas and water injectors for delaying gas and water breakthrough.
- Oil producers are located at some distance from major faults to avoid gas inflow.

B. Drilling and Completion Strategy

Three Well; B-2H, D-1H and D-2H, was drilled from the start-up in the C-segment field base case. These give plateau production in 2000. Two producers show good productivity and late gas break through. The last five were drilled continuously from the production start-up with a drilling time of 1-2 years until 2006. The four injectors are locations close to the edge of the simulation model rounding the in centre all the producers. The first injector well C-1H was drilled a year after the start-up of the field 1997, and follow by the other four injectors all drilled in 1998. The water injection wells has 5.5" and 7" tubing. The injection pressures are dependent on the bottom-hole pressure required to flow the water into the reservoir formation.

The wells are completed in different formations depending on the drainage strategy. The water injectors are perforated below the oil-water contact, and the two gas injectors are perforated in layer one top Garn formation. The vertical production wells are generally perforated in the Ile 1, top of Tofte 3 and Tofte. The production wells are completed to delay gas and water breakthrough and to minimize the amount of well interventions required [16].

C. Well Placement for Scenario 1 and 2

The objective was to place minimum number of wells to obtain same or higher recovery than the Statoil. A decision was made that 10 new wells will be placed taking well type, location and spacing in to consideration. In new well placement, the suffix "P" is used for producers and "I" is used for the injectors in both scenarios 1 and 2. The flow in the reservoir from the base case shows good recovery on both vertical and horizontal wells but high recovery is achieved with horizontal wells then the vertical wells. Since few wells will be placed to achieve high recovery, slant vertical wells and horizontal will be placed to decrease the drilling and operational cost.

D. Procedure

The base case wells were all removed from the Schedule file and the field was left with no wells accepts general reservoir properties. The flow pattern was studied along with oil/gas water saturation. New schedule files from Eclipse were formed and well placed continuously for each year starting with the P-1H to P-6H wells. First, by using keyword WELOPEN all existing injection wells were stopped and then opened only when observed pressure drop during production which are in both scenarios. Well properties in COMPDAT and WELSPECS keyword were on defaulted except wellbore.

To achieve a successful placement both for Scenario 1 and 2, several numbers of simulation runs was carried out and 6 successful producers, P-1H, P-2H, P-3H, P-4H, P-5H and P-6H, all horizontally placed for Scenario 1, while 4 producers, the remaining 2 producers were left in the same position as in Scenario 1, were placed for Scenario 2. The producer placement and completion are carry out where there is only high oil saturation in the field after

studying the direction of flow in the reservoir. The completions were targeted at the Ile and the Tofte formations which contain about 80% of the oil in Norne C-Segment.

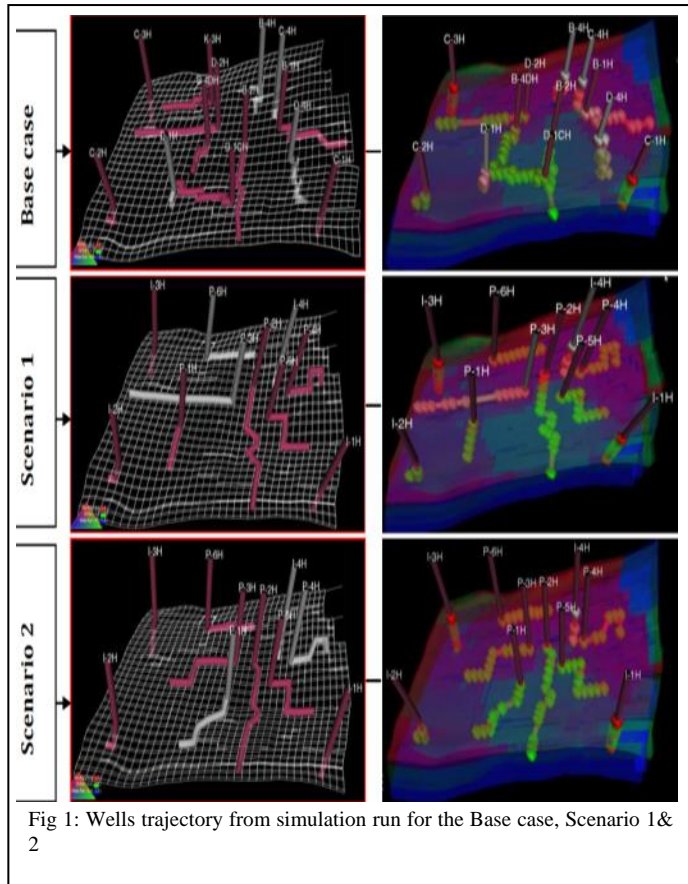


Fig 1: Wells trajectory from simulation run for the Base case, Scenario 1 & 2

The location of injection wells depends on the factor such as reservoir structure, injected fluid type, and displacement mechanism. Therefore, all injection wells, I-1H, I-2H, I-3H, and I-4H, in both scenario cases were left in the same location as in the base case. Injection wells are all vertical with perforation in the bottom for water injection and in the top for gas injection. Some of water injection wells are perforated throughout the reservoir. (See Figure 1 for the Wells trajectory from simulation run for the Base case, Scenario 1 & 2 in the Norne Field C-Segment.)

To decrease simulation time restart file for first 9 years of production was made. Then for each case including the base case, additional 9 years of production were simulated using Eclipse® software. Results of simulation were extracted from RSM files and compared between each other. In this part of report cases are compared only by using value of recovery factor. For economic calculation following indexes were extracted with time step of one year: cumulative oil production, cumulative water and gas injected. Description of the scenario cases and recovery factor after additional 9 years of production will be explain in as we go further on this work.

E. Production and injection constraints

A slight variation in Production and injection constraints is used in the simulation cases. For the

base case, maximum oil production rate for each oil producer is 7008 Sm³/day while the maximum oil production rate for each oil producer in scenario 1 and 2 is 8009 Sm³/day. Other production and injection constraints include;

- Maximum oil production rate for each oil producer is 7008 Sm³/day
- Maximum gas injection rate for each gas injector is 2600000 Sm³/day.
- Maximum water injection rate for each water injector is 3760 Sm³/day
- Maximum water-cut is 95%
- Maximum gas oil-ratio is 15675 Sm³/Sm³
- Maximum bottom-hole pressure is 376 bars

F. Reservoir Simulation Results and Discussions

The results obtained from simulation on base case field production and the scenario 1 and 2 well placement production and injection are presented and discussed. The results combine the initial production profile of the reservoir from 1997 to 2006 and the expected (forecast) production to 2015. Also the recoverable and unrecoverable reserves are summarised.

a. Oil Production Results

The Oil production in the base case from the year 1997 to 2006 is approximately 31.6 million Sm³. Oil production in case 1 is 34.3 million Sm³ and Scenario 2 is 36.7 million Sm³. Oil production forecast for the base case from 2006 to 2015 is estimated as 9.7 million Sm³. A total of 8.5 million Sm³ of oil is produced in this nine-year period in scenario 1 and 6.5 million Sm³ in scenario 2. The field oil production and the total oil production rate profiles for the three cases can be seen in Figure 2. The cumulative oil production rises from the base case to 41.3 million Sm³. The oil production for scenario case rises to 42.8 and 43.2 million Sm³ in scenario 1 & 2 cases. This shows that there is an increase of 1.5 to 1.9 million Sm³ of oil production for the two cases when compared to the base case.

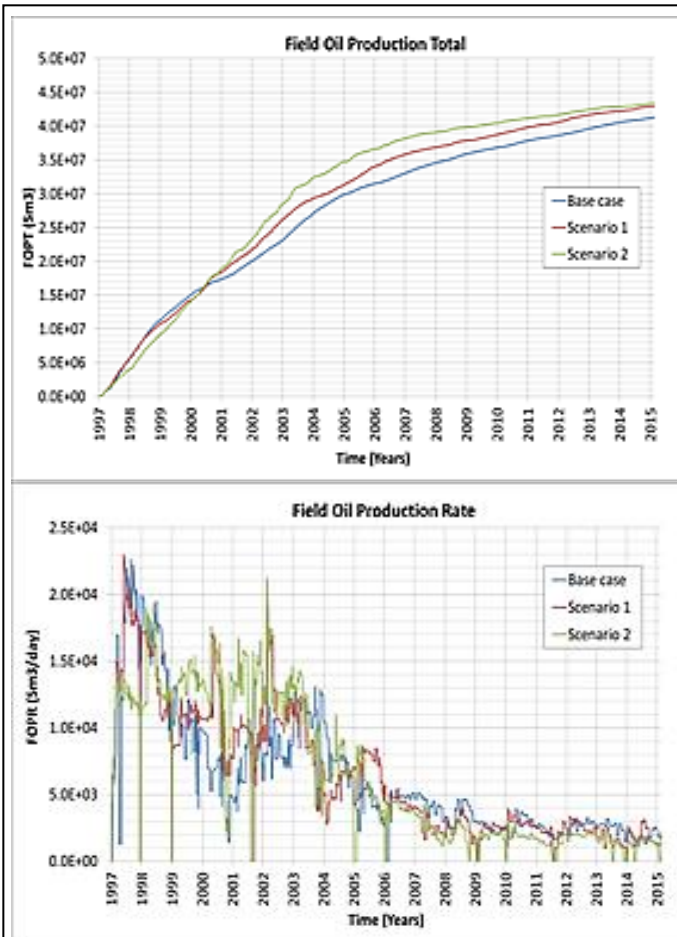


Fig 2: Field oil production rate and total field oil production profiles

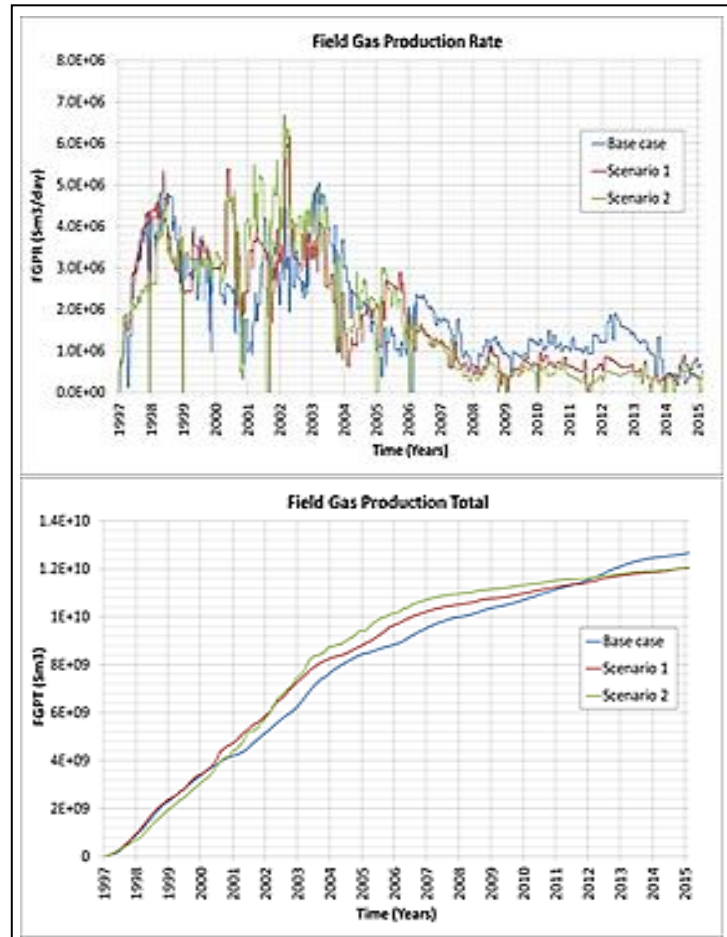


Fig 3: Field gas production rate and total field gas production profiles

b. Gas Production Results

The total volume of gas produced from the base case from 1997 to 2006 is 8.9 billion Sm³. However, the total produced gas for Scenario 1 is 9.7 billion Sm³ and scenario 2 produced 10.2 billion Sm³ of gas. The gas production forecast in the base case from 2006 to 2015 is 8.5 billion Sm³, while gas production for scenario 1 is 2.3 billion Sm³ and 1.8 billion Sm³ for scenario 2 case. The cumulative Gas production from 1997 to 2015 is therefore 12.7 billion Sm³ for the base case and 12.0 billion Sm³ for both Scenario 1 and 2. The production rate and total field gas production profiles can be seen in Figure 3.

c. Water production Results

The total water produced from the base case is 7.3 million Sm³. An approximately 6.1 million Sm³ of water is produced in scenario 1 and 3.7 million Sm³ in scenario 2 case. Water production forecast for base case in 2006 to 2015 is 16.0 million Sm³. A total of 15.5 million Sm³ of water is produced in this nine-year period in scenario 1 and 14.1 million Sm³ in scenario 2. The production rate and the total water production profiles from 1997 to 2015 can be seen in Figure 4. The cumulative water production rises from the base case to 23.3 million Sm³. For scenario 1, it rises to 21.6 million Sm³ and 17.8 million Sm³ for scenario 2 case.

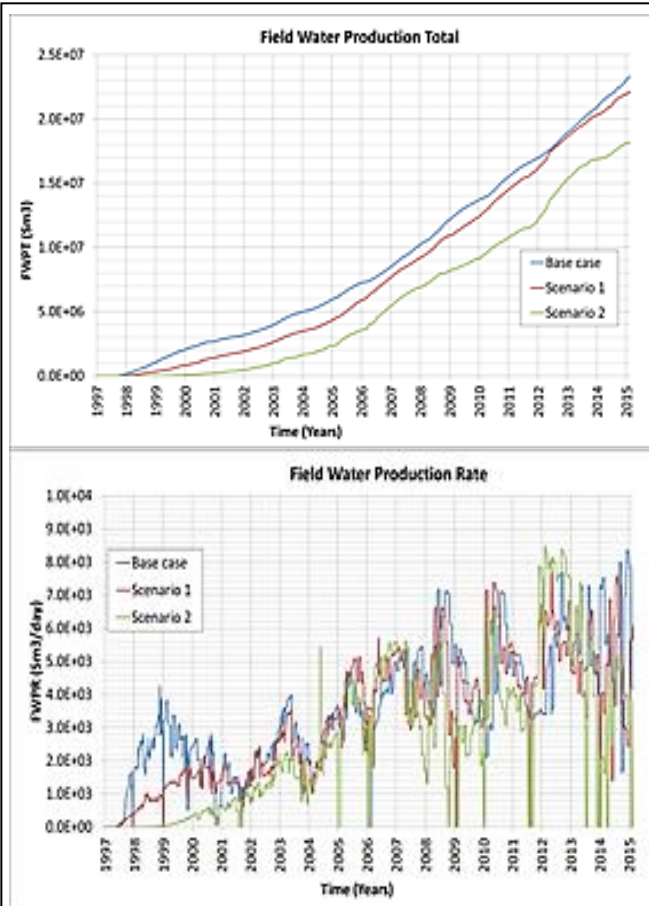


Fig 4: Water production rate and total field water production profiles

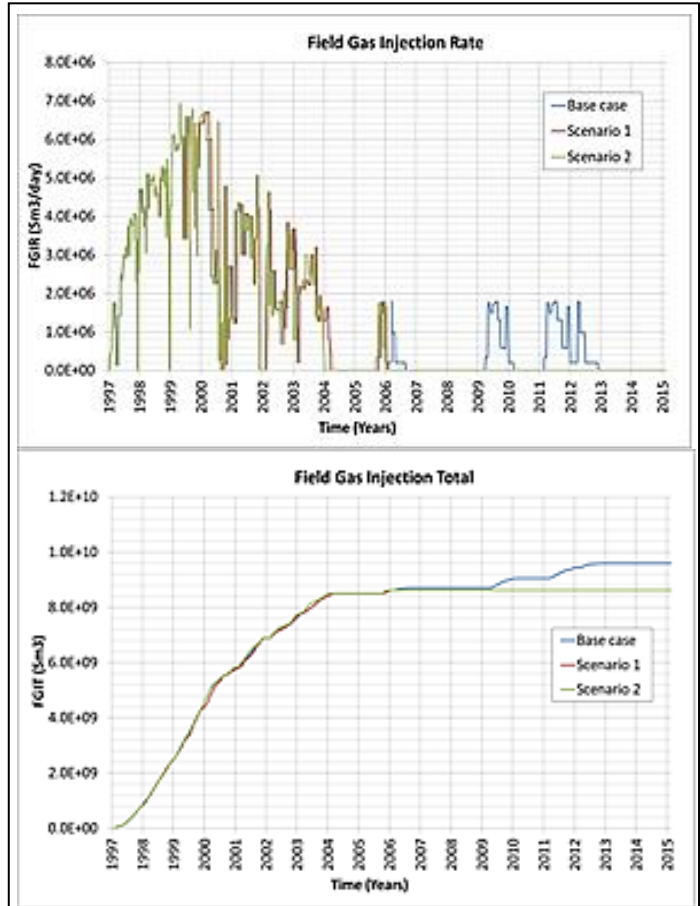


Fig 5: Field gas injection rate and total gas injection profiles

d. Gas injection and water injection

To improve the recovery of oil in the C-segment reservoir, the total volume of 8.63 billion Sm³ gas was injected in the base case and the same volume was also injected in scenario 1 and 2 from 1997 to 2006. From 2006 to 2015, gas injection to maintain pressure in the base case is 10 million Sm³ volume of gas, whereas the gas injection volume for each of the two scenarios are less than 1 million Sm³. Figure 5 presents the gas injection rate and the total field gas injection profiles for the three cases.

Water injection from 1997 to 2015 in the base case is 79million Sm³. Injected water estimated in scenario 1 & 2 from 1997 to 2015 is 81.2 million Sm³ for each case. Figure 6 shows the water injection rate and the total field water injection profiles for the three cases.

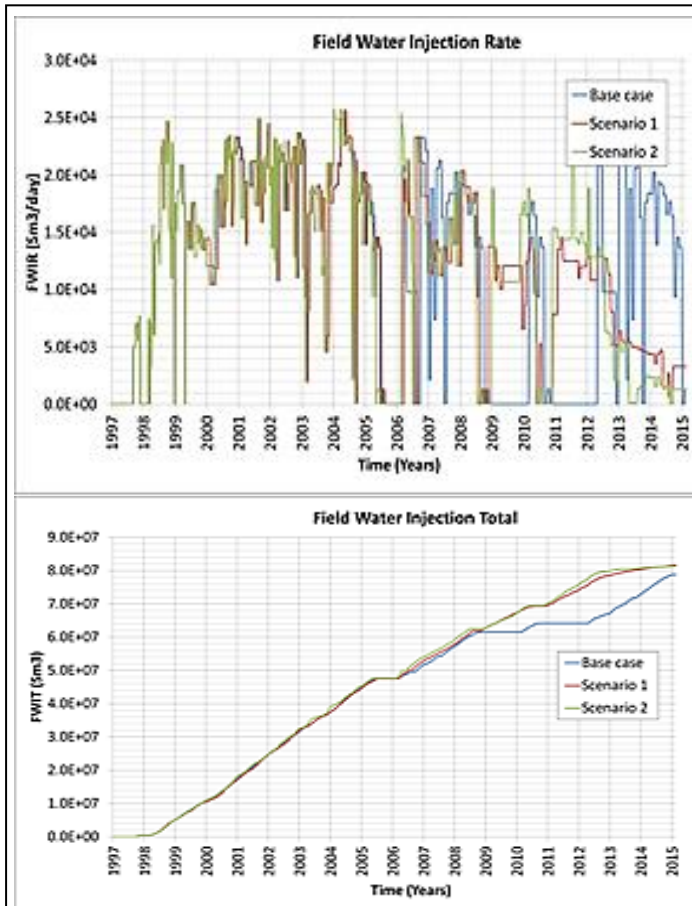


Fig 6: Field water injection rate and the total water injection profiles

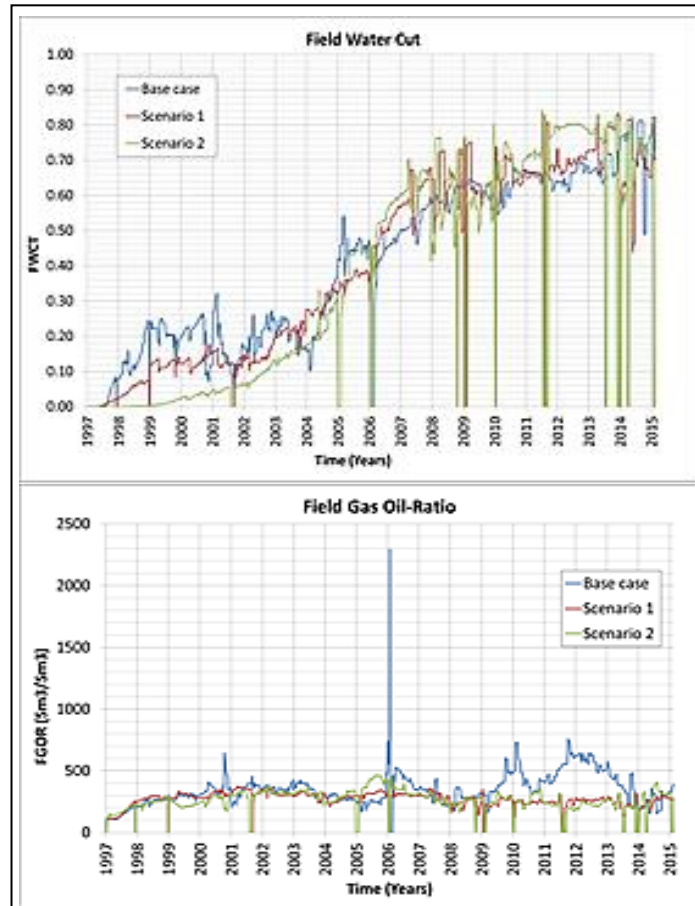


Fig 7a: Field Water-cut and Gas-Oil Ratio profile

e. Oil Recovery

Oil recovery factor for the base case is 21.4%, Scenario 1 has 23.2% oil recovery factor and Scenario 2 is 24.9%. From 1997 to 2015, the forecasted oil recovery factor for the base case increased to 28.0% while oil recovery factor is 29.0% for scenario1 and 29.3% for scenario 2. (See figure 7a); The field water-cut, GOR. Oil recovery efficiency and the field reservoir pressure profiles for the three scenarios are also presented in figure 7b,

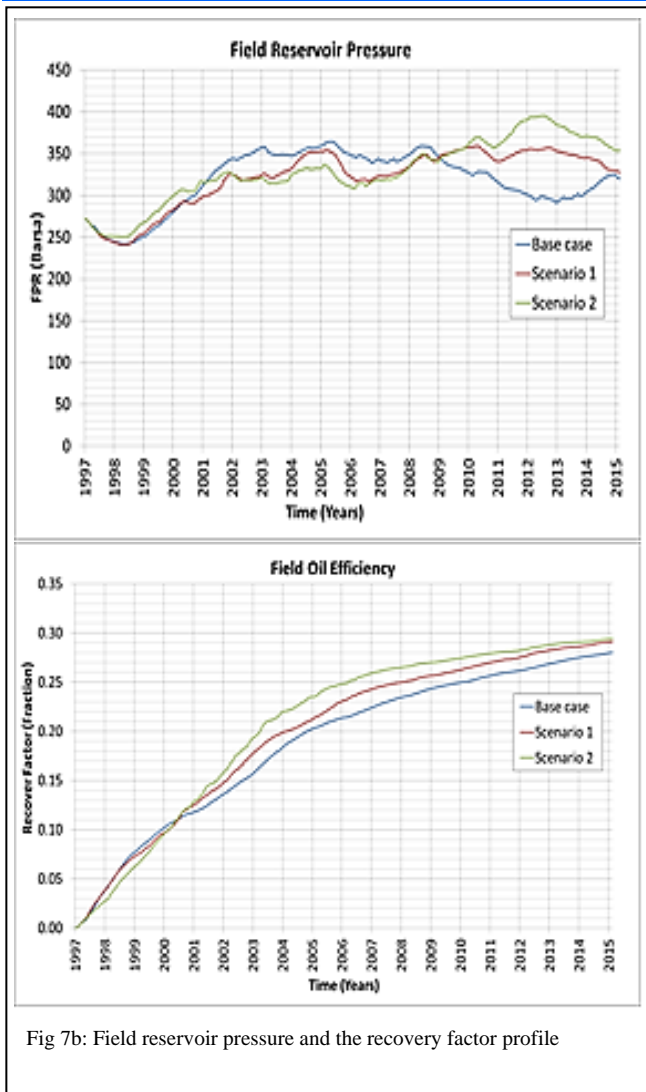


Fig 7b: Field reservoir pressure and the recovery factor profile

G. Recoverable and Unrecoverable reserves

Originally, oil in-place in the simulations model is estimated as 147 million Sm³ and gas in place as 230 billion Sm³ in 1997. The recoverable oil reserves, the recoverable gas reserves and the unrecoverable reserves for the three cases, from 1997 to 2015, are presented in table 1.

Table 1: Reserves of Oil and Gas in the C-segment Field from 1997 to 2015

Description	Units	Base case	Scenario 1	Scenario 2
Oil in Place, STOIP	* 10 ⁶	147.6	147.6	147.6
Gas in Place (free & Solution)	* 10 ⁹	229.9	229.9	229.9
Recoverable Oil Reserves	* 10 ⁶	41.4	43.0	43.4
Recoverable Gas Reserves	* 10 ⁹	3.06	3.35	3.37
Unrecoverable Oil reserved	* 10 ⁶	106.2	104.6	104.2

IV. ECONOMIC ANALYSES

A. Net Present Value (NPV)

Present value of money compares the value of a certain amount of money today to the value of that same amount in the future and vice versa, taking into

consideration inflation and returns. Net present value (NPV) is the difference between the present value of cash inflow and the present value of cash outflow. Given an investment opportunity, NPV is used by an organization to analyze the profitability of the project or investment and to make decisions with regards to capital budgeting. It is sensitive to the future cash inflows that an investment or project will yield [17].

Table 2: Economic assumptions for NPV calculation

Economic Parameter	Cost (USD)
Vertical well	
Cost of drilling a vertical well	17000000
Capital expenditure (CapEx) per vertical well	1700000
Operating Expenditure (OpEx) per vertical well	800000
Horizontal wells	
Cost of drilling a horizontal well	20000000
Capital expenditure (CapEx) per horizontal well	2000000
Operating Expenditure (OpEx) per horizontal well	1000000
Fixed parameters	
Fixed Capital expenditure	200000000
Fixed Operating expenditure per year	5000000
Other operational costs were not taken into consideration:	
Cost of Gas injection Per MSCf	\$12
Cost of water injection Per Mbbl	\$8
Discount rate	8%
Inflation rate	8%
Oil price	\$25 and \$35

Thus, the objective is to calculate the net present value over the life of the reservoir and this is achieved after generating the results of the reservoir simulation. In carrying out this analysis, a number of assumptions are made. The economic parameters assumed can be seen in Table 2 below.

The calculation of NPV is possible after extracting results to a user friendly Excel Spread sheet program from the simulation output file. Annual oil production, summation of oil produced from the wells in a year for each case, represents a single value. NPV takes more consideration of the economics of the project period, starting with the first year of production 1997-2006 until the forecast production period 2015 (See Table 3).

The base case will be compared with other Scenario case. The NPV formula used is given below;

Formula:

$$NPV = \sum_{t=0}^n \left(\frac{CF_t}{(1+d)^t} \right) \quad (1)$$

Where: CF_t = Cash Flow of a period "t"

d = Discount rate for period "t"

n = Last period of economic horizon

Cash flow is cash inflow minus cash outflow. The main elements required for a cash flow analysis are: Revenue, $R = \text{Production} \times \text{Price}$, and Expenditure, $E = \text{Operating expenditure (OPEX)} + \text{capital expenditure (CAPEX)}$. The investment Decision is if $\text{NPV} > 0$, the Project is accepted or $\text{NPV} < 0$, the Project is rejected. This means the project with the highest NPV is favorable.

In any petroleum project, the price of crude oil is very important. Oil prices changing with respect to time, in the fore-casting of oil price, inflation needs to be factored into the estimates. Hence, inflation is used to calculate current price value of 1997 to 2015. The assume oil prices based on 1997 are \$25 as low price, \$35 as high price. The rate of inflation is stated as a percentage. This represents the rate of changes of prices between the current and previous year. Thus, Inflation;

$$I = P_0(1 + R)^n(2)$$

Where, I is an inflation index

P_0 , Initial oil Price (based on 1997)

R , inflation rate per annum

n , the number of years

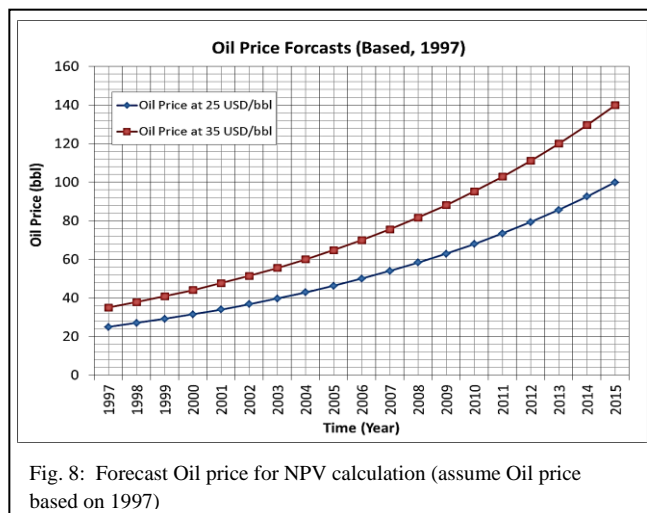


Fig. 8: Forecast Oil price for NPV calculation (assume Oil price based on 1997)

Using the above equation, the result for the forecast oil price is presented in Figure 8.

For economic calculation, the oil production is converted from standard cubic feet (Sm³) to barrel (bbl). The conversion factor is given in table 4. A detailed economic analysis is carried out in excel sheet. Tables 5 through 9 at the Appendix present the cost of gas and water injection, well cost and total expenditure for base case wells and the new well case scenario 1 & 2. NPV calculation for all cases is shown in Tables 10 through 12, lastly NPV results summary for the three cases at different oil price value presented in Table 13. Figure 9 shows the NPV comparisons for the three cases at the price regimes under study.

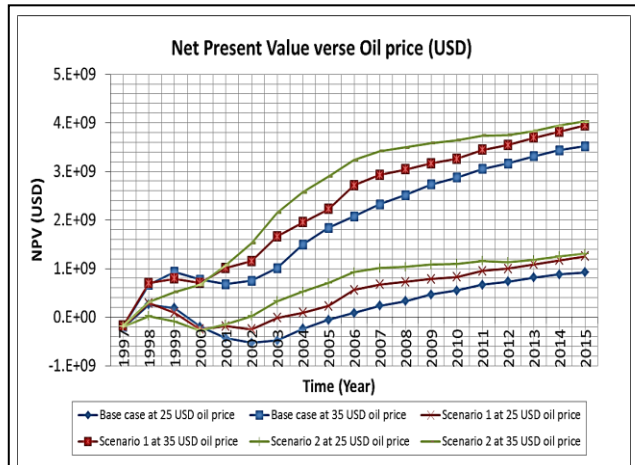


Fig. 9: Summary of NPV comparisons for base case and the two scenarios at various Oil price values

The Net present value for the three project for the base case, scenario 1 & 2 at low oil price; \$25, slightly high oil price; \$35, is presented below in Table 14.

Table 14: The Net Present Value

Present Value (PV)	Oil price at 25 USD (mill)	Oil price at 35 USD (mill)
Base case	918	3,516
Scenario 1	1,254	3,945
Scenario 2	1,307	4,026

The NPV show values in relative to the oil prices, the higher the oil price, the higher the NPV. Base on economic decision, all cases are considered since there is no negative NPV. However, the NPV for the base case is less when compare to scenario 1 & 2; the NPV of scenario 1 is less than that of scenario 2. The best case is thus scenario 2.

V. CONCLUSION

The Norne field is the largest discovery on the Norwegian continental shelf in more than a decade with recoverable oil reserves of 450 Million bbl, and has four main fault blocks of C, D, E and G segment. Maximum oil production can be obtained with more oil wells, but few optimal numbers of wells in good location reduces economic costs and increase recovery. The Norne field C-segment reservoir model in Eclipse® software is used to study the effect of well placement. Six producers (while the four injectors remain the same as those of the base case) for two different well placement scenarios, 1 and 2, are located manually after identifying grid blocks with high oil saturation.

Oil recovery factor for the base case is 21.4%, Scenario 1 has 23.2% oil recovery factor and Scenario 2 is 24.9%. From 1997 to 2015, the forecasted oil recovery factor for the base case increased to 28.0% while oil recovery factor is 29.0%

for scenario 1 and 29.3% for scenario 2. The cumulative Gas production from 1997 to 2015 is therefore 12.7 billion Sm³ for the base case and 12.0 billion Sm³ for both Scenario 1 and 2. From 1997 to 2015, the cumulative water production rises from the base case to 23.3 million Sm³. For scenario 1, it rises to 21.6 million Sm³ and 17.8 million Sm³ for scenario 2 case. Water injection from 1997 to 2015 in the base case is 79 million Sm³. Injected water estimated in scenario 1 & 2 from 1997 to 2015 is 81.2 million Sm³ for each case.

From the economic analyses, the NPV for the base case is less when compare to scenario 1 & 2; the NPV of scenario 1 is less than that of scenario 2. The best case is thus scenario 2.

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Norwegian petroleum sector, collective from (1997- 2010).

Table 3: Cumulative Oil Production for Base case and Scenario Cases (in Sm3 and bbl)

	Cum.Oil Prod.(Sm ³)	Cum.Oil Prod.(Sm ³)	Cum.Oil Prod.(Sm ³)	Cum.Oil Prod.(bbl)	Cum.Oil Prod.(bbl)	Cum.Oil Prod.(bbl)
Year	Base case	Scenario 1	Scenario 2	Base case	Scenario 1	Scenario 2
1997	384337	293356	306413	2417481	1845209	1927340
1998	6139044	6308123	4387918	38614586	39678094	27600002
1999	5329219	4553771	5052367	33520788	28643220	31779388
2000	3635180	3916340	5358832	22865282	24633779	33707053
2001	2114810	3966190	4352620	13302155	24947335	27377980
2002	2795720	3204060	4477600	17585079	20153537	28164104
2003	3356280	4413450	5021370	21111001	27760601	31584417
2004	3837120	2867970	3623370	24135485	18039531	22790997
2005	2507320	2188040	2310810	15771043	13762772	14534995
2006	1465200	2557960	1838920	9216108	16089568	11566807
2007	1700750	1583690	1505740	10697718	9961410	9471105
2008	1449620	1009530	877030	9118110	6349944	5516519
2009	1299620	988210	703930	8174610	6215841	4427720
2010	894290	793770	627940	5625084	4992813	3949743
2011	1046370	1033440	660850	6581667	6500338	4156747
2012	754400	759330	439670	4745176	4776186	2765524
2013	1024350	984500	702160	6443162	6192505	4416586
2014	908990	697280	568860	5717547	4385891	3578129
2015	664020	654230	415130	4176686	4115107	2611168
	41306640	42773240	43231530	259818766	269043680	271926324

Table 4: Conversion Factor [18]

Nomenclature	Units
CapEx Capital Expenditure	rcf Reservoir cubic feet
OpEx Operating Expenditure	res.bbl Reservoir barrel
3D Three Dimensions	rm3 Reservoir cubic metres
NPV Net Present Value	scf Standard cubic feet
Np Cumulative Oil Produced	sm3 Standard cubic metres
	Mscf 1000 scf
	MMscf 1000000 scf
Subscript	stb Stock tank barrel
o Original	\$ (USD) Dollars
i Initial	bbl Barrel
g Gas	bcf Billion Cubic Feet
w Water	d Day

Conversion Factor

1 Sm3 Oil	=	1.0	Sm3o.e.
1000 Sm3 Gas	=	1.0	Sm3o.e.
1 Sm3Condensate	=	1.0	Sm3o.e.
1 tonne NGL	=	1.9	Sm3o.e.
1 Sm3 Crude Oil	=	6.29	barrels
1 Sm3 Crude Oil	=	0.84	tonnes Crude Oil
1 Sm3 Gas	=	35.314	Scf

Table 5: Cost of Gas injection (in USD/Sm3 and USD/Scf)

Year	Total Gas Injected (Sm ³)	Total Gas Injected (Sm ³)	Total Gas Injected (Sm ³)	Costs of Gas Injection (USD/Scf)	Costs of Gas Injection (USD/Scf)	Costs of Gas Injection(USD /Scf)
	Base case	Scenario1	Scenario2	Base case	Scenario1	Scenario2
1997	27068270	25636610	31295750	955888887	905331246	1105178116
1998	1047243730	1048675390	1035985250	36982365081	37032922722	36584783119
1999	1657076000	1670657000	1667069000	58517981864	58997581298	58870874666
2000	2170290000	2154696000	2349805000	76641621060	76090934544	82981013770
2001	948453000	950466000	853363000	33493669242	33564756324	30135660982
2002	1043499000	1050320000	974221000	36850123686	37091000480	34403640394
2003	873764000	866945000	879802000	30856101896	30615295730	31069327828
2004	716852000	715147000	718664000	25314911528	25254701158	25378900496
2005	25959000	27662000	0	916716126	976855868	0
2006	123771000	118666000	118666000	4370849094	4190571124	4190571124
2007	70404000	0	0	2486246855	0	0
2008	0	0	0	0	0	0
2009	0	0	0	0	0	0
2010	353277000	0	0	12475623978	0	0
2011	1120000	0	0	39551680	0	0
2012	391197000	0	0	13814730858	0	0
2013	147179000	0	0	5197479206	0	0
2014	0	0	0	0	0	0
2015	0	0	0	0	0	0
	9597153000	8628871000	8628871000	60366092370	54275598590	54275598590

Table 6: Cost of Water Injection (in Sm3 and bbl)

Year	Total Water Injected (Sm ³)	Total Water Injected (Sm ³)	Total Water Injected (Sm ³)	Costs of Water Injection (\$/bbl)	Costs of Water Injection (\$/bbl)	Costs of Water Injection (\$/bbl)
	Base case	Scenario1	Scenario2	Base case	Scenario1	Scenario2
1997	0	0	0	0	0	0
1998	465521	465521	465521	2928125	2928125	2928125
1999	5434252	5475522	5443252	34181448	34441036	34238058
2000	5611987	5567587	5948987	35299398	35020122	37419128
2001	7059300	7062430	7098850	44402997	44422685	44651767
2002	6964340	7095900	6801140	43805699	44633211	42779171
2003	7200530	7069010	7180550	45291334	44464073	45165660
2004	5658350	5638240	6676880	35591022	35464530	41997575
2005	7411840	7431910	6687070	46620474	46746714	42061670
2006	1810130	1713130	1501380	11385718	10775588	9443680
2007	4607690	5533470	6328420	28982370	34805526	39805762
2008	5881330	4980280	5208850	36993566	31325961	32763667
2009	3385690	4678230	3205540	21295990	29426067	20162847
2010	0	4371820	4214260	0	27498748	26507695
2011	2701040	2204000	2700120	16989542	13863160	16983755
2012	0	4260820	5545750	0	26800558	34882768
2013	4032220	4394590	4532530	25362664	27641971	28509614
2014	5640200	2068220	1045800	35476858	13009104	6578082
2015	4973990	1207780	590300	31286397	7596936	3712987
	78838410	81218460	81175200	495893599	510864113	510592008

Table 7a: Well cost and total expenditures for Base case, Scenario 1 & 2 wells

Year of well Placement	Nos of Vertical well	CapEx. for Vertical wells + Cost of drilling Vertical well	CapEx. + Drilling costs for Vertical and Horizontal wells	Nos. of Vertical well* OpEx. per Vertical wells (USD)	OpEx. + Drilling costs for Vertical and Horizontal
1997	1	18700000	60700000	800000	2800000
1998	3	52700000	54700000	2400000	2400000
1999	3	52700000	74700000	2400000	3400000
2003	0	1700000	23700000	0	1000000
2004	0	1700000	23700000	0	1000000
2006	1	18700000	20700000	800000	800000
Total	8	146200000	258200000		11400000
Numbers of wells and Expenditures in Scenario-1 wells					
1997	1	18700000	20700000	800000	800000
1998	1	18700000	80700000	800000	3800000
1999	3	52700000	74700000	2400000	3400000
2003	0	1700000	23700000	0	1000000
Total	5	91800000	177800000		9000000
Numbers of wells and Expenditures in Scenario-2 wells					
1997	0	1700000	23700000	0	1000000
1998	1	18700000	40700000	800000	1800000
1999	3	52700000	74700000	2400000	3400000
2001	0	1700000	23700000	0	1000000
2002	0	1700000	23700000	0	1000000
2003	0	1700000	23700000	0	1000000
Total	4	78200000	210200000		9200000

Table 7b: Cont. on Well cost and total expenditures for Base case, Scenario 1 & 2 wells

Year of well Placement	Nos of Horizontal well	CapEx. for Horizontal wells + Cost of drilling Horizontal well	CapEx. + Drilling costs for Vertical and Horizontal wells	No. of Horizontal well * OpEx. Per Horizontal wells (USD)	OpEx. + Drilling costs for Vertical and Horizontal
1997	2	42000000	60700000	2000000	2800000
1998	0	2000000	54700000	0	2400000
1999	1	22000000	74700000	1000000	3400000
2003	1	22000000	23700000	1000000	1000000
2004	1	22000000	23700000	1000000	1000000
2006	0	2000000	20700000	0	800000
Total	5	112000000	258200000		11400000
Numbers of wells and Expenditures in Scenario-1 wells					
1997	0	2000000	20700000	0	800000
1998	3	62000000	80700000	3000000	3800000
1999	1	22000000	74700000	1000000	3400000
2003	1	22000000	23700000	1000000	1000000
Total	5	86000000	177800000		9000000
Numbers of wells and Expenditures in Scenario-2 wells					
1997	1	22000000	23700000	1000000	1000000
1998	1	22000000	40700000	1000000	1800000
1999	1	22000000	74700000	1000000	3400000
2001	1	22000000	23700000	1000000	1000000
2002	1	22000000	23700000	1000000	1000000
2003	1	22000000	23700000	1000000	1000000
Total	6	132000000	210200000		9200000

Table 12a: Net Present Value Calculation for Base Case

NPV for Base Case with Oil Price at 25 USD						
Year	Year	Cum. Oil Production (bbl)	Oil Price at 25 (USD/bbl)	Revenue (USD)	CapEx = Fixed CapEx + CapEx per well + Well cost (USD)	OpEx Fixed OpEx + Total Cost of Gas + Water injection (USD)
1997	0	2417481	25.0	60437025	260700000	7800000
1998	1	38614586	27.0	1042593809	54700000	7400000
1999	2	33520788	29.2	977466164	74700000	8400000
2000	3	22865282	31.5	720091759	0	5000000
2001	4	13302155	34.0	452435872	0	5000000
2002	5	17585079	36.7	645956250	0	5000000
2003	6	21111001	39.7	837512643	23700000	6000000
2004	7	24135485	42.8	1034099490	23700000	6000000
2005	8	15771043	46.3	729777489	0	5000000
2006	9	9216108	50.0	460576063	20700000	5800000
2007	10	10697718	54.0	577389243	0	5000000
2008	11	9118110	58.3	531503510	0	5000000
2009	12	8174610	63.0	514626453	0	5000000
2010	13	5625084	68.0	382452805	0	5000000
2011	14	6581667	73.4	483290781	0	5000000
2012	15	4745176	79.3	376312519	0	5000000
2013	16	6443162	85.6	551847544	0	5000000
2014	17	5717547	92.5	528875687	0	5000000
2015	18	4176686	99.9	417252947	0	5000000

NPV for Base case with Oil Price at 25 USD

Year	Year	Total Expenditure (CapEx + OpEx) (USD)	Cash Flow (USD)	Present Value (PV) (USD)	Net Present Value (USD)
1997	0	279970667	-219533642	-219533642	-219533642
1998	1	529313378	513280431	475259658	255726016
1999	2	1058767363	-81301199	-69702674	186023342
2000	3	1207094639	-487002879	-386598587	-200575245
2001	4	762148007	-309712135	-227647665	-428222910
2002	5	797647073	-151690823	-103238225	-531461135
2003	6	762303892	75208751	47394271	-484066864
2004	7	618207110	415892379	242669209	-241397655
2005	8	388964382	340813107	184130717	-57266938
2006	9	170035931	290540133	145342401	88075463
2007	10	266693923	310695320	143912049	231987512
2008	11	300948526	230554984	98881081	330868593
2009	12	175367921	339258532	134724231	465592824
2010	13	154707488	227745317	83741480	549334304
2011	14	141390953	341899828	116403571	665737875
2012	15	170776770	205535748	64793440	730531315
2013	16	270271061	281576483	82189491	812720806
2014	17	288814864	240060823	64880987	877601793
2015	18	255291177	161961771	40530776	918132569
Total			2725782929	918132569	

Table 12b: Cont. on Net Present Value Calculation for Scenario 1 Case

NPV for Scenario 1 with Oil Price at 25 USD								NPV for Scenario 1 with Oil Price at 25 USD					
Year	Year	Cum. Oil Production (bbl)	Oil Price at 25 (USD/bbl)	Revenue (USD)	CapEx = Fixed CapEx + CapEx per well + Well cost (USD)	OpEx		Year	Year	Total Expenditure (CapEx + OpEx) (USD)	Cash Flow (USD)	Present Value (PV) (USD)	Net Present Value (USD)
						Fixed OpEx per well (USD)	Total Cost of Gas + Water injection (USD)						
1997	0	1845209	25.0	46130215	220700000	5800000	10863975	1997	0	237363975	-191233760	-191233760	-191233760
1998	1	39678094	27.0	1071308546	807000000	8800000	467820069	1998	1	557320069	513988477	475915256	284681497
1999	2	28643220	29.2	835236283	747000000	8400000	983499263	1999	2	1066599263	-231362979	-198356464	86325033
2000	3	24633779	31.5	775786663	0	5000000	1193252192	2000	3	1198252192	-422465530	-335366758	-249041725
2001	4	24947335	34.0	848514350	0	5000000	758158553	2001	4	763158553	85355796	62739058	-186302667
2002	5	20153537	36.7	740303959	237000000	6000000	802157694	2002	5	831857694	-91553736	-62309934	-248612601
2003	6	27760601	39.7	1101314603	0	5000000	723096132	2003	6	728096132	373218471	235190945	-13421656
2004	7	18039531	42.8	772914663	0	5000000	586772651	2004	7	591772651	181142013	105694625	92272968
2005	8	13762772	46.3	636848243	0	5000000	385695982	2005	8	390695982	246152262	132988408	225261376
2006	9	16089568	50.0	804078042	0	5000000	136491555	2006	9	141491555	662586487	331458206	556719582
2007	10	9961410	54.0	537648432	0	5000000	278444210	2007	10	283444210	254204221	117745740	674465322
2008	11	6349944	58.3	370144409	0	5000000	250607690	2008	11	255607690	114536719	49122836	723588158
2009	12	6215841	63.0	391313620	0	5000000	235408534	2009	12	240408534	150905087	59926486	783514644
2010	13	4992813	68.0	339464338	0	5000000	219989982	2010	13	224989982	114474355	42091983	825606627
2011	14	6500338	73.4	477318754	0	5000000	110905280	2011	14	115905280	361413474	123047208	948653834
2012	15	4776186	79.3	378771719	0	5000000	214404462	2012	15	219404462	159367257	50239206	998893040
2013	16	6192505	85.6	530379174	0	5000000	221135769	2013	16	226135769	304243405	88805750	1087698790
2014	17	4385891	92.5	405696916	0	5000000	104072830	2014	17	109072830	296624085	80168280	1167867070
2015	18	4115107	99.9	411101165	0	5000000	60775490	2015	18	65775490	345325676	86417415	1254284485
								Total		3226921781	1254284485		

Table 12c: Cont. on Net Present Value Calculation for Scenario 2 Case

NPV for Scenario 2 with Oil Price at 25 USD								NPV for Scenario 2 with Oil Price at 25 USD					
Year	Year	Cum. Oil Production (bbl)	Oil Price at 25 (USD/bbl)	Revenue (USD)	CapEx = Fixed CapEx + CapEx per well + Well cost (USD)	OpEx		Year	Year	Total Expenditure (CapEx + OpEx) (USD)	Cash Flow (USD)	Present Value (PV) (USD)	Net Present Value (USD)
						Fixed OpEx per well (USD)	Total Cost of Gas + Water injection (USD)						
1997	0	1927340	25.0	48183491	223700000	6000000	13262137	97	0	242962137	-194778646	-194778646	-194778646
1998	1	27600002	27.0	745200063	407000000	6800000	462442394	98	1	509942394	235257669	217831175	23052529
1999	2	31779388	29.2	926686967	747000000	8400000	980354957	99	2	1063454957	-136767990	-117256507	-94203978
2000	3	33707053	31.5	106152949	0	5000000	1295125191	00	3	1300125191	-238595704	-189404962	-283608940
2001	4	27377980	34.0	931185982	237000000	6000000	718842064	01	4	748542064	182643918	134248732	-149360208
2002	5	28164104	36.7	1034557719	237000000	6000000	755077050	02	5	784777050	249780670	169996527	20636318
2003	6	31584417	39.7	1253012520	237000000	6000000	734157210	03	6	763857210	489155311	308250820	328887138
2004	7	22790997	42.8	976494107	0	5000000	640527408	04	7	645527408	330966700	193115890	522003028
2005	8	14534995	46.3	672581529	0	5000000	336493362	05	8	341493362	331088167	178876635	700879663
2006	9	11566807	50.0	578052508	0	5000000	125836295	06	9	130836295	447216213	223719449	924599111
2007	10	9471105	54.0	511185112	0	5000000	318446094	07	10	323446094	187739017	86959490	1011558602
2008	11	5516519	58.3	321563253	0	5000000	262109332	08	11	267109332	54453921	23354353	1034912955
2009	12	4427720	63.0	278743786	0	5000000	161302773	09	12	166302773	112441013	44651873	1079564828
2010	13	3949743	68.0	268545342	0	5000000	212061563	10	13	217061563	51483779	18930479	1098495307
2011	14	4156747	73.4	305229233	0	5000000	135870038	11	14	140870038	164359195	55957903	1154453210
2012	15	2765524	79.3	219317769	0	5000000	279062140	12	15	284062140	-64744371	-20410126	1134043084
2013	16	4416586	85.6	378274292	0	5000000	228076910	13	16	233076910	145197383	42381732	1176424816
2014	17	3578129	92.5	330978585	0	5000000	52624656	14	17	57624656	273353929	73879080	1250303895
2015	18	2611168	99.9	260856926	0	5000000	29703896	15	18	34703896	226153030	56594576	1306898471
								tal		2846403202	1306898471		

Table 13a: Summary of Net Present Value Result for Base case

Table 13a: Summary of Net Present Value Result for Base case

NPV (USD) for Base case			
Year	Cum.Oil Prod.(bbl)	Base case at 25 USD Oil price	Base case at 35 USD Oil price
1997	2417481	-219533642	-195358832
1998	38614586	255726016	666046681
1999	33520788	186023342	931551882
2000	22865282	-200575245	773606117
2001	13302155	-428222910	678980001
2002	17585079	-531461135	751592564
2003	21111001	-484066864	1010096847
2004	24135485	-241397655	1494120904
2005	15771043	-57266938	1835962049
2006	9216108	88075463	2073465530
2007	10697718	231987512	2324354754
2008	9118110	330868593	2514416933
2009	8174610	465592824	2730887262
2010	5625084	549334304	2870879583
2011	6581667	665737875	3053099827
2012	4745176	730531315	3165345027
2013	6443162	812720806	3311966133
2014	5717547	877601793	3434022591
2015	4176686	918132569	3516320225

Table 13b:Cont. on Summary of Net Present Value Result for scenario 1

NPV (USD) for Scenario 1			
Year	Cum.Oil Prod. (bbl)	Scenario 1 at 25 USD Oil price	Scenario 1 at 35 USD Oil price
1997	1845209	-191233760	-172781674
1998	39678094	284681497	699914526
1999	28643220	86325033	787990258
2000	24633779	-249041725	698961286
2001	24947335	-186302667	1011173695
2002	20153537	-248612601	1150399135
2003	27760601	-13421656	1663196085
2004	18039531	92272968	1949286022
2005	13762772	225261376	2219902146
2006	16089568	556719582	2712256036
2007	9961410	674465322	2929615877
2008	6349944	723588158	3042238150
2009	6215841	783514644	3164323045
2010	4992813	825606627	3256343161
2011	6500338	948653834	3444393744
2012	4776186	998893040	3542394807
2013	6192505	1087698790	3693125607
2014	4385891	1167867070	3817152799
2015	4115107	1254284485	3944721281

Table 13c: Cont. on Summary of Net Present Value Result for Scenario 2 case

NPV (USD) for Scenario 2			
Year	Cum. Oil Prod. (bbl)	Scenario 2 at 25 USD Oil price	Scenario 2 at 35 USD Oil price
1997	1927340	-194778646	-175505249
1998	27600002	23052529	318325949
1999	31779388	-94203978	518863326
2000	33707053	-283608940	666528897
2001	27377980	-149360208	1074557427
2002	28164104	20636318	1526194993
2003	31584417	328887138	2150289986
2004	22790997	522003028	2571315849
2005	14534995	700879663	2895542433
2006	11566807	924599111	3234929949
2007	9471105	1011558602	3416600486
2008	5516519	1034912955	3495120026
2009	4427720	1079564828	3584049096
2010	3949743	1098495307	3642477001
2011	4156747	1154453210	3740002369
2012	2765524	1134043084	3747247486
2013	4416586	1176424816	3833795082
2014	3578129	1250303895	3943455455
2015	2611168	1306898471	4026161708